



Operational data and model extension

Alan Foster (*LSBU*)



This project has received funding from the European Union's Horizon 2020 Research and Innovation Programme under Grant Agreement No 691761.

17th March 2021

Current round trip efficiency (RTE)

Output

129 kW cooling to warehouse (equiv. 51 kW electrical)

45 kW electrical power (turbines)

Input

0.42 kg/s LIN (2.13 MW)

6 kW fan power

RTE 4.5%

Includes

Electricity generated, cooling to warehouse, warehouse fan power.

Doesn't include

Defrosts, start-up and shutdown losses, Interstage cooling from turbines (-30 to -40°C).

Assumes

COP of ammonia refrigeration (-30°C) = 2.5

Energy cost of LIN = 1.4 kWh/kg (Claude cycle LN system limited to 200 Bara pressure, LIN Pressure 17 Bara)



Original concept

Original concept was to recover cold energy between turbines (turbine reheat) using a heat transfer fluid to a chilled warehouse.

Ammonia condensers (warehouse refrigeration) were used due to cost of HXs.

Assuming all cold recovered from before turbines to chilled warehouses (30 kW of chilled cooling).

RTE = 4.9%

Assumes

COP of 4 at -10°C





Design specification



Pressure (bara)	Design	Actual
After pump	15.4	16.3
Before Turbine 1	14.8	15.4
Before Turbine 2	6.4	6.7
Before Turbine 3	2.5	2.7



Turbine efficiency (%)	Design	Actual
Turbine 1	79	53
Turbine 2	81	61
Turbine 3	74	64



RTE = 5.5 %

Pump to higher pressure



Pump pressure (bara)	RTE (%)
15	5.5
30	6.0
60	6.3
75	5.7

Assumes

25% pump efficiency

If we had a liquefaction system and recycled the cold (15 bar)

RTE = 14 %

Assumes

Cold energy storage efficiency = 91 %

15 bar pressure

No waste/recovered heat



Recycled and waste heat (30 bar)

	RTE (%)
Heat recycle from liquefier @ 230°C	31
+ waste heat @ 350°C	38
+ waste heat @ 550°C	49
+ waste heat @ 650°C	55
+ waste heat @ 750°C	61

Assumes

30 bara LA storage and let-down pressures
(no LA pump)



Conclusions

Demonstrator system

RTE low - Energy cost of liquefaction much higher than energy production from turbines and value of cooling to cold store warehouse

Ideal system

Reduce liquefaction cost

Connected to liquefaction system via thermal store

Use cold at lower temperatures

Cryogenic freezers

Increase power generation

Recycle heat from liquefaction system via thermal store

Further high temperature process waste heat

Higher pressures and more efficient turbines and pumps





**For further information:
Alan Foster:
alan.foster@lsbu.ac.uk**



This project has received funding from the European Union's Horizon 2020 Research and Innovation Programme under Grant Agreement No 691761.